

Short communication

Improved high power Li-ion batteries with Li_2RuO_3 addition: A fast charging and fast cycling study

Arnold M. Stux*, Karen E. Swider-Lyons

Code 6113, Naval Research Laboratory, Washington, DC 20375, USA

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Abstract

The high-rate charging and cycling of Li-ion batteries is improved by blending Li_2RuO_3 into LiCoO_2 cathodes in cells with $\text{Li}_4\text{Ti}_5\text{O}_{12}$ anodes. The cathode-limited cells have greater discharge capacities when Li_2RuO_3 -containing cathodes are recharged up to 2C rates. The $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{Li}_2\text{RuO}_3 + \text{LiCoO}_2$ cells also show capacity increases over initial cycles and minimal capacity decay when cycled at a 2C rate over 50 cycles. These benefits are attributed to the reduced cell impedance of the Li_2RuO_3 -containing cathodes.

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1. Introduction

Miniaturized rechargeable lithium-ion batteries are attractive power sources for autonomous microdevices because of their high specific energy, long cycle life, and minimal electronic disruption to microelectronic systems. These devices typically require high energy and high power, plus capability for rapid recharging. High power and rapid recharging are a challenge because the capacities of Li-ion cells decrease with increasing discharge and charge rates. We have previously shown that the specific power and energy at high cycling rates, such as 2C, is improved by the addition of Li_2RuO_3 to LiCoO_2 in the cathodes of Li-ion batteries with carbonaceous anodes [1]. Blended cathodes of LiCoO_2 and Li_2RuO_3 were particularly effective; combining these insertion materials so that they were electrically in parallel resulted in reduced cell impedance and low IR losses in the cells.

Li_2RuO_3 is a stable Li^+ insertion compound with high electronic and Li-ion conductivity and high volumetric capacity [2–4]. Physical mixing of Li_2RuO_3 and another Li^+ insertion material is a favorable approach because it utilizes both the low resistivity of Li_2RuO_3 and the reversibility of Li^+ insertion and de-insertion. In pure Li_2RuO_3 electrodes, the $\text{Ru}^{5+/4+}$ redox couple permits facile Li^+ liberation. Approximately one mole of Li^+

is extracted per mole Li_2RuO_3 within common testing voltage ranges. Li_2RuO_3 has two voltage plateaus at both 3.6 and 3.4 V, which had been correlated to two distinct biphasic regimes [2]. The 3.6 V plateau corresponds to compositions of $0.7 < x < 1.0$ in $\text{Li}_{2-x}\text{RuO}_3$.

One approach to improving the charging rate capability of Li-ion batteries is to use $\text{Li}_4\text{Ti}_5\text{O}_{12}$ as the active material in the anode [5]. The reduction potential of $\text{Li}_4\text{Ti}_5\text{O}_{12}$ is 1.5 V versus Li^+/Li , so it does not form a resistive solid electrolyte interphase (SEI) layer, which impedes charging and discharge rates [5,6]. The 1.5 V potential also eliminates any risk of Li metal plating during fast charging. $\text{Li}_4\text{Ti}_5\text{O}_{12}$ is often selected in conjunction with experimental ionic liquid-based electrolytes in order to avoid cathodic decomposition of the electrolyte solvent during cycling [7,8]. $\text{Li}_4\text{Ti}_5\text{O}_{12}$ also exhibits no dimensional changes with Li^+ intercalation, and is available in nano-sized particles. Its fine particles allow diffusion of Li^+ over small distances in and out of the host lattice structure [6,9]. Selection of LiFePO_4 cathodes with $\text{Li}_4\text{Ti}_5\text{O}_{12}$ anodes has been recently promoted because LiFePO_4 is environmentally friendly and inexpensive. One criticism of the $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiFePO}_4$ cells is that they have low voltage—about 2.0 V. Moreover, the conductivity of LiFePO_4 is poor, although some measures have been taken to increase the conductivity with dispersion of carbon [10]. Higher cell voltages of 2.4 V are obtained when the $\text{Li}_4\text{Ti}_5\text{O}_{12}$ is coupled with LiCoO_2 [11], a somewhat expensive but well-performing and commercially successful Li-ion battery cathode material. For microdevices,

* Corresponding author. Tel.: +1 202 404 3340; fax: +1 202 404 8119.
E-mail address: arnold.stux@nrl.navy.mil (A.M. Stux).

high power performance can be more important than materials cost.

This investigation shows how engineering the cathode formulation can improve the charging rate capability of Li-ion batteries beyond simple use of $\text{Li}_4\text{Ti}_5\text{O}_{12}$ anodes. Detailed rate studies are used to demonstrate the effects of the addition of Li_2RuO_3 to LiCoO_2 -based cathodes. Our method is to charge cells at different rates but to discharge them at the slower rate of $C/5$. Each discharge profile is affected by its preceding recharge rate. We present an approach that involves cathode-limited cells with $\text{Li}_4\text{Ti}_5\text{O}_{12}$ anodes, maintains nearly 2.4 V plateaus, and further improves recharge capability. Specifically, we compare cells with and without Li_2RuO_3 in the cathode for both rapid recharge up to $2C$ and rapid cycling at $2C$ in cathode-limited Li-ion cells.

2. Experimental

2.1. Materials

Li_2RuO_3 was synthesized by mixing commercially available powders of RuO_2 and Li_2CO_3 following previously described procedures [2,3]. Briefly, hydrous RuO_2 (Alfa Aesar) was dried at 400°C for 18 h to remove structural water. Afterwards, the RuO_2 was ground together with an equimolar amount of Li_2CO_3 (Alfa Aesar), pelletized, and sintered in air at 950°C for 24 h. The pellets were then pulverized using an agate mortar and pestle and sieved to approximately $30\ \mu\text{m}$. Commercially available LiCoO_2 was used as the standard cathode active material.

Cathodes were prepared using LiCoO_2 or a 60:40 (w/w) mixture of LiCoO_2 and Li_2RuO_3 , respectively, as the active Li^+ insertion constituent of the slurry. Anodes of $\text{Li}_4\text{Ti}_5\text{O}_{12}$ (NEI, less than 500 nm particles) were similarly prepared.

2.2. Electrode fabrication

The active materials were formulated into slurries using previously developed recipes [12]. The cathode slurries were a mixture of approximately 91 wt% active cathode material, 2% Super P carbon (Ensaco), 4% KS6 carbon (Timcal), and 3% polyvinylidene fluoride (PVDF, Atofina). The carbon additives were ground with the active material or stirred in the slurry. The PVDF was dissolved separately in 1-methyl-2-pyrrolidone (NMP, Aldrich) and then combined with the active material/carbon powders to make viscous ink for efficient deposition. For the Li-ion cells, anode slurries were prepared from 87% $\text{Li}_4\text{Ti}_5\text{O}_{12}$, 1.5% Super P carbon, and 8.5% PVDF dissolved in NMP. An ink was prepared from 10% Super P carbon and 90% PVDF in NMP to serve as a conductive coating and adhesion layer to the current collectors.

The slurries were deposited on current collectors of aluminum and copper foils (All-Foils, Inc.) approximately $4\ \text{mm} \times 4\ \text{mm}$ in area. The Al and Cu foils were pre-treated by etching with 1 M potassium hydroxide and 1 M nitric acid solutions, respectively, followed by rinsing with water and then acetone. A layer of the conductive carbon ink was then added to their surfaces. The conductive coating/adhesion layer was dried

on a hot plate at the lowest heat setting for approximately 1 min in order to obtain a homogeneous film. The anode and cathode slurries were then deposited on the carbon-coated Cu and Al foils, respectively. The electrodes were subsequently dried again on the hotplate, and then vacuum-dried overnight $90\text{--}95^\circ\text{C}$ before transferring to an argon-filled glove box. The electrodes were not calendered or pressed. Cells were constructed with weight ratios of positive to negative active materials so that the capacity was limited by the active material in the cathode. The weight of the active materials was 0.6–0.8 mg for the cathodes used with Li anodes. The weights of the active materials in the cathodes were 0.3–0.5 mg and those of the $\text{Li}_4\text{Ti}_5\text{O}_{12}$ in the anodes were 0.4–0.6 mg. For Li test cells, metallic Li foil was fixed to the Cu foil to form the anode, whereby the Li could be used as both a counter and a reference electrode.

2.3. Electrochemical investigation

The LiCoO_2 and Li_2RuO_3 cathode blends were evaluated in packaged Li-ion cells at room temperature both using metallic Li and $\text{Li}_4\text{Ti}_5\text{O}_{12}$. The electrolyte was 1 M LiPF_6 in a mixture of carbonates containing ethylene carbonate, propylene carbonate, ethyl methyl carbonate, and diethyl carbonate. The Li-ion micro-batteries, or small packaged cells, were assembled using the procedures described previously [12]. A microporous polymer film (Celgard 2730) was used as a separator and sandwiched between the LiCoO_2 /carbon/aluminum and $\text{Li}_4\text{Ti}_5\text{O}_{12}$ /carbon/copper electrodes. The cathode/separator/anode sandwiches were first held together by impulse sealing them in a transparent polymer bag (Saranex SX 23-P), followed by sealing in another pouch of a tri-layer polyethylene–aluminum–polyester. During the sealing process, small holes were left in the polymer seals to allow electrolyte injection. After the battery was filled with the electrolyte, the pouch was fully sealed. With this packaging process, the Li-ion batteries were protected from ambient air and gently held together with no additional pressure on the electrodes.

The electrochemical testing of Li-ion cells was conducted using a battery tester (Maccor 2300) set to cut-off voltages. For cells with the $\text{Li}_4\text{Ti}_5\text{O}_{12}$ anodes, the cut-off voltages were 1.1 and 2.75 V. For cells with the Li anodes, the cut-off voltages were 2.5 and 4.15 V. Cells were cycled at $C/5$, charged at various rates with intermittent $C/5$ discharge, and then cycled at $2C$. The charge rates with intermittent $C/5$ discharges were $C/5$, $C/3$, $C/2$, C , $3C/2$, and $2C$ corresponding to constant currents ranging from 0.15 to $1.5\ \text{mA cm}^2$. For the blends, appropriate currents were determined by normalizing the weighted averages of the single-component specific capacities of discharge at $C/5$ rates. The test current densities were adjusted according to the total mass of active material(s), and the specific capacities initially measured for LiCoO_2 ($122\ \text{mAh g}^{-1}$) and Li_2RuO_3 ($140\ \text{mAh g}^{-1}$).

3. Results

3.1. Fast charging

Fig. 1 shows the charge and discharge profiles of the $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiCoO}_2$ cells. In this figure, “time zero” begins after

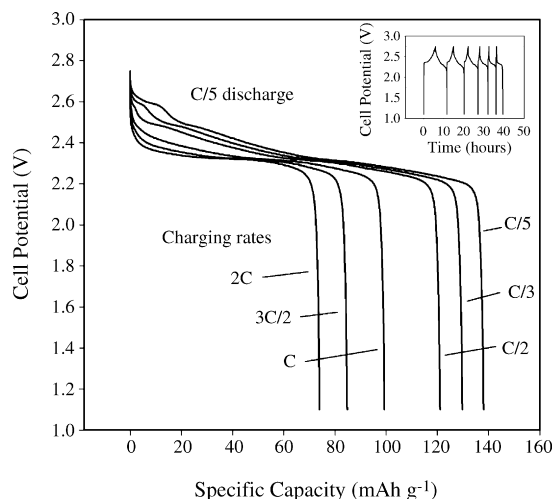


Fig. 1. Discharge profiles of $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiCoO}_2$ cells discharged at $C/5$ but preceded by indicated charge rates of $C/5$, $C/3$, $C/2$, C , $3C/2$, and $2C$ rates but with $C/5$ discharge rates. The inset shows the cycling profile of $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiCoO}_2$ with successive charging of $C/5$, $C/3$, $C/2$, C , $3C/2$, and $2C$ rates but with $C/5$ discharge rates.

the fifth $C/5$ cycle and at the beginning of the rate study. The $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{Li}_2\text{RuO}_3 + \text{LiCoO}_2$ cell in Fig. 2 has additional lower voltage plateaus in the discharge profiles near 2.0 V, corresponding to insertion and de-insertion of Li^+ in and out of Li_2RuO_3 . Visual comparison of the figures reveals that the $C/5$ discharge times of the $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiCoO}_2$ cells decrease more with increasing charge rates than those of the $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{Li}_2\text{RuO}_3 + \text{LiCoO}_2$ cell.

The $C/5$ discharge profiles for the same $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiCoO}_2$ and $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{Li}_2\text{RuO}_3 + \text{LiCoO}_2$ cells in Figs. 1 and 2 are insets and show how varying the recharge rates from $C/5$ to $2C$ between 1.1 and 2.75 V affects the capacity of the $C/5$ discharge. For both types of cells, the voltage plateaus are flat at potentials of 2.4 V with respect to the Li/Li^+ potential when $\text{Li}_4\text{Ti}_5\text{O}_{12}$

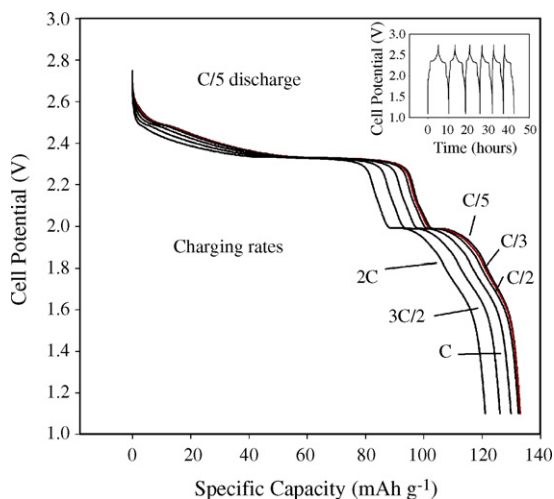


Fig. 2. Discharge profiles of $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiCoO}_2 + \text{Li}_2\text{RuO}_3$ cells discharged at $C/5$ but preceded by indicated charge rates of $C/5$, $C/3$, $C/2$, C , $3C/2$, and $2C$ rates but with $C/5$ discharge rates. The inset shows the cycling profile of $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiCoO}_2 + \text{Li}_2\text{RuO}_3$ cells with successive charging of $C/5$, $C/3$, $C/2$, C , $3C/2$, and $2C$ rates but with $C/5$ discharge rates.

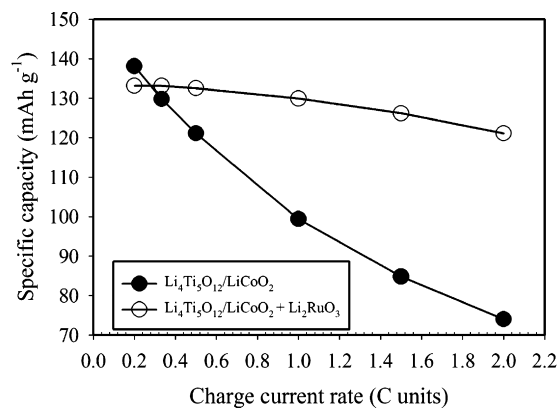


Fig. 3. Comparison of $C/5$ discharge capacities of $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiCoO}_2$ and $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiCoO}_2 + \text{Li}_2\text{RuO}_3$ cells as a function of charge rate.

is used as the anode. The $C/5$ discharge capacities following $C/5$, $C/3$, and $C/2$ charging are 138, 129, and 121 mAh g^{-1} for the $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiCoO}_2$ cell but are all 133 mAh g^{-1} for the $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{Li}_2\text{RuO}_3 + \text{LiCoO}_2$ cell. The decrease in the $C/5$ discharge capacity, with the testing protocol described in Section 2.3, is less for the $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{Li}_2\text{RuO}_3 + \text{LiCoO}_2$ cells than for the $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiCoO}_2$ cells. For the pure LiCoO_2 cathode, despite starting at 2.75 V, the initial voltages of the discharge curves decrease with an increase of the preceding charge rate, indicating initial drop to a lower state of charge. The $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{Li}_2\text{RuO}_3 + \text{LiCoO}_2$ cells maintain flat discharge curves even with increasing recharge rates, indicating little ohmic loss.

Fig. 3 summarizes the data in Figs. 1 and 2 and demonstrates that the specific capacity of the $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiCoO}_2$ cells discharged at a $C/5$ rate decreases more with charging rate than the $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{Li}_2\text{RuO}_3 + \text{LiCoO}_2$ cells.

Fig. 4 shows discharge profiles for cells with metallic Li anodes and $\text{Li}_2\text{RuO}_3 + \text{LiCoO}_2$ cathodes. The shapes of the curves are similar to those of the $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{Li}_2\text{RuO}_3 + \text{LiCoO}_2$ cells. The plateaus corresponding to insertion and de-insertion of Li^+ in and out of Li_2RuO_3 are prominent in these Li-cells and show no decrease in these cycles, while the capacity associated

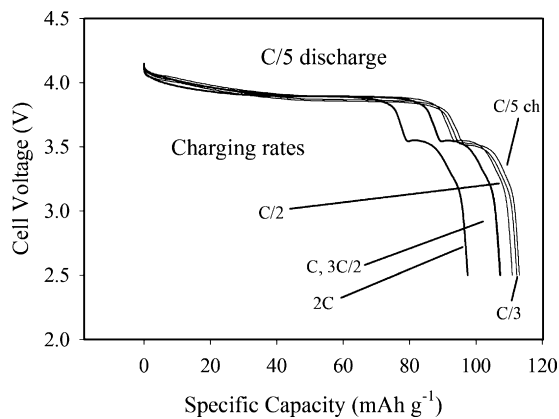


Fig. 4. Discharge profiles of lithium cells, comprised of $\text{LiCoO}_2:\text{Li}_2\text{RuO}_3$ 60:40 (w/w) cathodes and metallic Li anodes, discharged at $C/5$ followed by indicated charge rates.

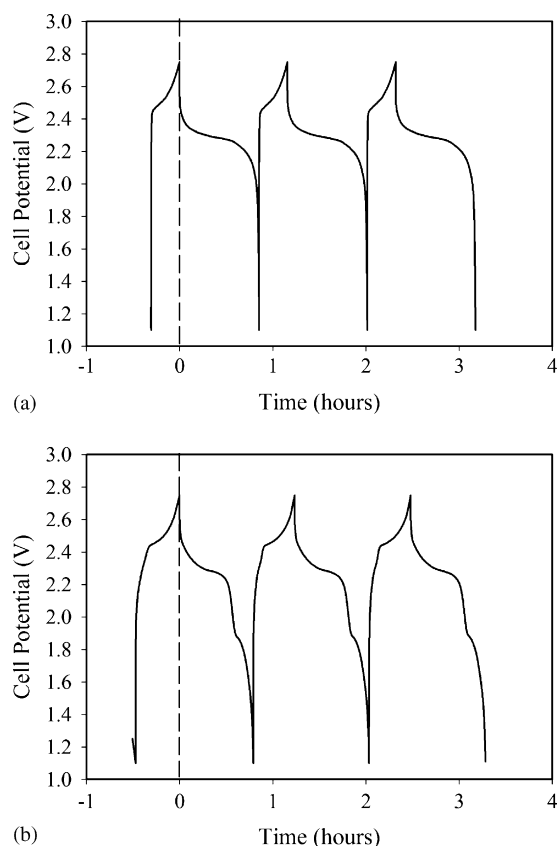


Fig. 5. Cycling profile of (a) $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiCoO}_2$ cells and (b) $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiCoO}_2 + \text{Li}_2\text{RuO}_3$ at 2C rate.

with LiCoO_2 shows marked decrease with increasing recharge rate.

3.2. Fast cycling

Fig. 5 shows representative 2C charge–discharge cycles of $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiCoO}_2$ and $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{Li}_2\text{RuO}_3 + \text{LiCoO}_2$ cells after completion of the varied rate tests shown in Figs. 1 and 2. The specific capacities increase over the first 12 cycles before

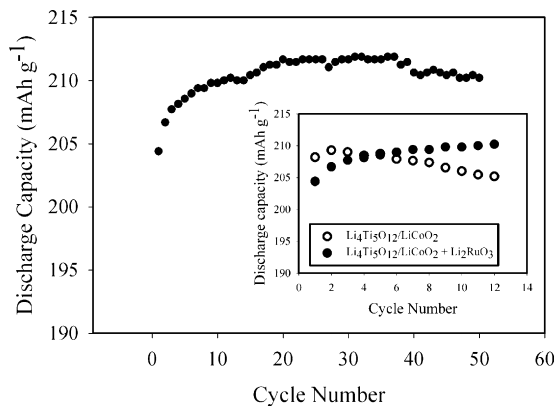


Fig. 6. Discharge capacities of $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiCoO}_2 + \text{Li}_2\text{RuO}_3$ as a function of cycle number. Inset: Comparison of initial specific capacities on discharge for cells cycled at 2C, both with $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiCoO}_2 + \text{Li}_2\text{RuO}_3$ and $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiCoO}_2$ cells.

levelling off for the $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{Li}_2\text{RuO}_3 + \text{LiCoO}_2$ cell, whereas fade begins immediately after the first cycle at the 2C rate with the $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiCoO}_2$ cell. Fig. 6 shows the specific capacities of $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{Li}_2\text{RuO}_3 + \text{LiCoO}_2$ cells for up to 50 cycles. The inset shows a comparison of the trends in capacities for cells using these two types of cathodes. The fade rate is generally lower for the $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{Li}_2\text{RuO}_3 + \text{LiCoO}_2$ cells than the $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{LiCoO}_2$ cells. The cells with Li_2RuO_3 as one of the active cathode materials have superior cycling durability to those without.

4. Discussion

The addition of Li_2RuO_3 to LiCoO_2 cathodes enhances the ability for fast charging and fast cycling of Li-ion cells with $\text{Li}_4\text{Ti}_5\text{O}_{12}$ anodes. Generally, the discharge capacities of Li-ion cells decrease with both increasing discharge and recharge rates. This trend is mitigated in the $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{Li}_2\text{RuO}_3 + \text{LiCoO}_2$ cells because Li_2RuO_3 is a low-impedance material, allows fast charging without a deleterious effect to the discharge capacity, and causes the blend to have less polarization. The impedance of cells with electrodes containing Li_2RuO_3 as part or all of the active material was shown previously to be lower than cells with pure LiCoO_2 -based cathodes [1]. Li_2RuO_3 improves the electrochemical kinetics of cells with LiCoO_2 because Li_2RuO_3 has a low resistivity of $10 \Omega \text{cm}$ [13]. Li_2RuO_3 also promotes the utility of LiCoO_2 by virtue of only its conductive properties, creating a more extensive conductive network and enhancing the interparticle electronic conductivity of LiCoO_2 , as RuO_2 does in V_2O_5 [14] and LiMn_2O_4 [15]. Also, there is extra capacity at 2.0 V with the testing cut-off voltages for the $\text{Li}_4\text{Ti}_5\text{O}_{12}/\text{Li}_2\text{RuO}_3 + \text{LiCoO}_2$ cell, even with the C/2 and 2C rates, because of the Li_2RuO_3 .

The Li_2RuO_3 additionally enhances electrode utility as evidenced by the increasing specific capacity over the first 12 2C-rate cycles for the cell using the cathode blend (Fig. 6). This supports early reports of kinetically fast electrochemical delithiation from Li_2RuO_3 [4]. It further suggests cation disorder and movement of Ru to different lattice sites within the LiRu_2 layers upon deintercalation of Li^+ . In situ X-ray diffraction at various states of charge may be needed to probe this further.

Percolation networks also play a role because the effect reported in this study relies on optimization of connectivity. It is likely that adjustments to the materials' particle size, morphology, and their relative concentration (or volume) can be made to further improve the performance of the electrodes. The use of nanoparticles in the cathode blends can also improve the performance as ionic conductivity can increase with decreasing particle size, although the electronic conductivity may decrease [16]. Although Li_2RuO_3 is acceptable for applications requiring small amounts of active material, such as microbatteries, its benefit might not be economically viable for large batteries due to the high cost of ruthenium. Nevertheless, lessons can be applied to other low-impedance materials.

5. Conclusions

The rate and power capability of Li-ion batteries with $\text{Li}_4\text{Ti}_5\text{O}_{12}$ anodes are increased by blending Li_2RuO_3 into the LiCoO_2 cathodes. The Li_2RuO_3 and LiCoO_2 are combined in parallel via a physical mixing or blending of the two Li^+ insertion materials. An improvement in capacity is shown during both rapid recharging and fast cycling testing procedures. The $\text{Li}_2\text{RuO}_3 + \text{LiCoO}_2$ cells can be implemented on a small scale with $\text{Li}_4\text{Ti}_5\text{O}_{12}$ for high power 2.4 V cells with no addition to standardized processes other than the preparation of Li_2RuO_3 .

Acknowledgments

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